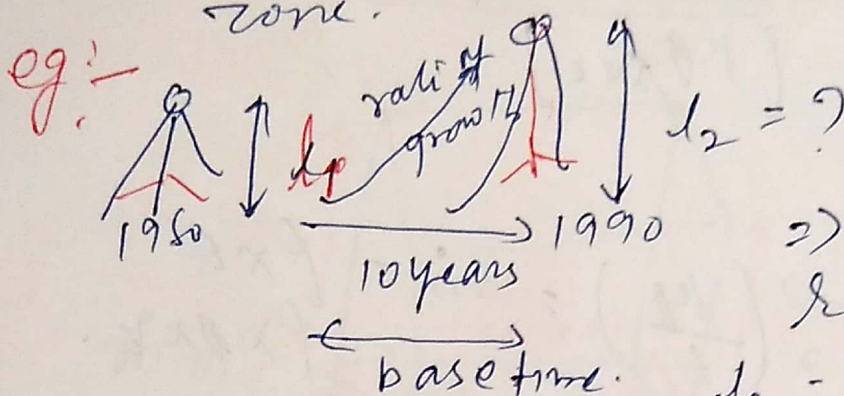
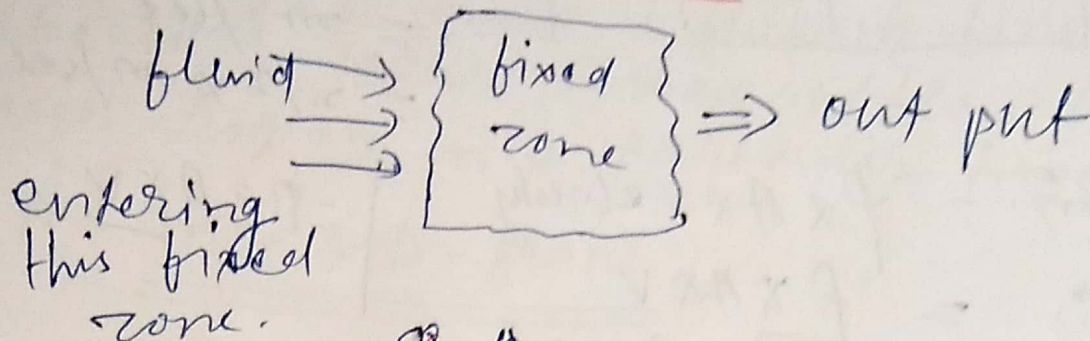


* continuity equation *

* conservation of mass *



$$\Rightarrow l_1 + (\Delta l)$$

$$\text{rate} = (x) \frac{\text{cm}}{\text{year}}$$

$$l_2 = l_1 + \text{rate of growth} \times \text{base time}$$

$$(x) \frac{\text{cm}}{\text{year}} \times 10 \text{ years}$$

$$\Rightarrow l_1 + \left(\frac{\partial l}{\partial y} \right) \times (dy)$$

$\frac{\partial l}{\partial y}$ rate of growth
 (dy) change in year
partial differential

$\Rightarrow$ continuity equation $\rightarrow$

conservation of mass *

mass = ~~kg~~ $\cdot$ sec.

$\rightarrow$ In fluid mechanics mass rate is observed instead of only mass.

* mass rate $\rightarrow$ mass per unit time.

$$\dot{m} = \rho \times \text{discharge}$$

$$\boxed{\dot{m} = \rho \times Q}$$

$$\begin{aligned} Q &= \text{Area} \times \text{velocity} \\ &= \text{m}^2/\text{sec} \\ &= \text{m}^2 \times \text{m}/\text{sec} \end{aligned}$$

$$\dot{m} = \rho \times A \times \text{velocity}$$

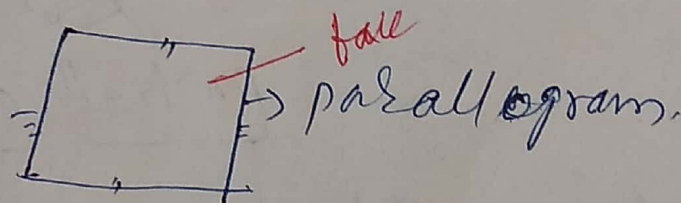
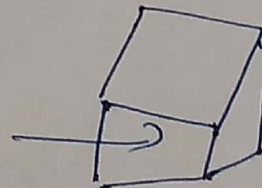
$$\dot{m} = \rho \times A \times v$$

$$Q = A \times v$$

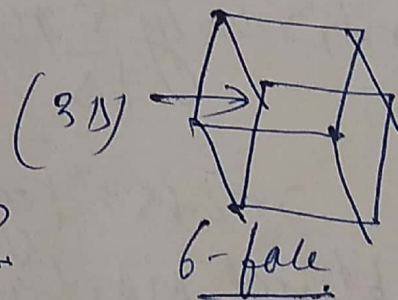
$$\boxed{\dot{m} = \rho \times Q} \quad (\text{kg/sec})$$

$$\begin{aligned} \frac{\text{kg}}{(\text{+})} &\rightarrow \left(\frac{\text{kg}}{\text{+}} \right) = \dot{m} = \rho \times Q \\ &= \rho \times A \times v \end{aligned}$$

* * parallelepiped $\rightarrow$



* parallelepiped (3D)

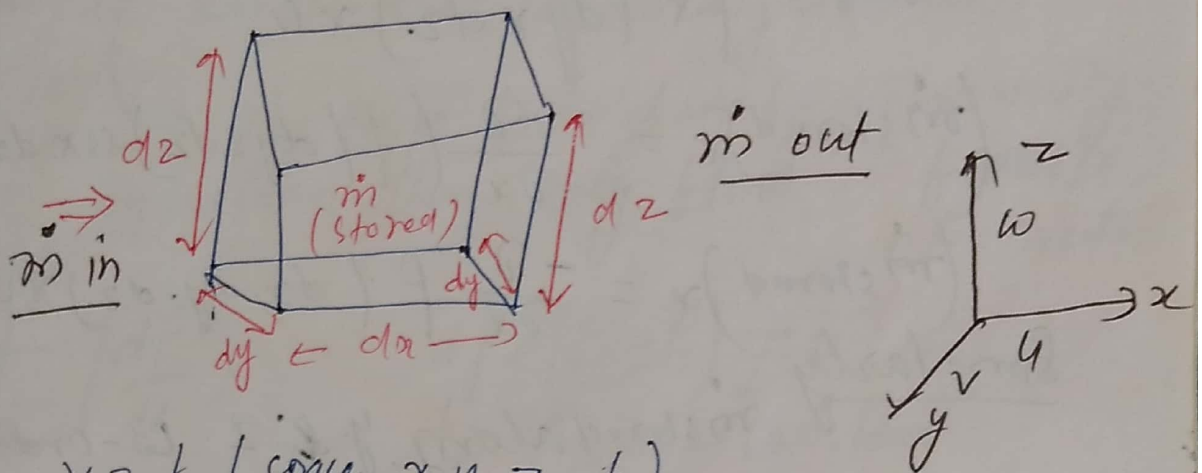


$\rightarrow$ using - 6 - parallelogram

* Continuity equation *

→ It is based on Principle of conservation of mass i.e. mass inflow in fixed region should be equal to mass outflow from that fixed region in a particular time.

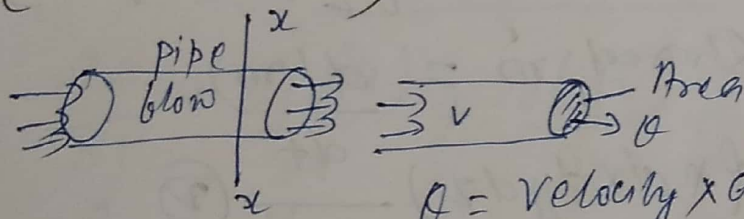
* in 3-D-flow



$$v = f(\text{space}, x, y, z, t)$$

$$\vec{v} = u\vec{i} + v\vec{j} + w\vec{k} \quad \text{where } \vec{i} = \text{unit vector in } x\text{-direction.}$$

$$(\dot{m}_{in} - \dot{m}_{out}) = \dot{m}_{stored}$$



$\dot{m} = \text{velocity} \times \text{area}$
cross-sectional area of flow.

* in x-direction

$$(\dot{m}_{in})_x - (\dot{m}_{out})_x = (\dot{m})_{x, stored}$$

$$\begin{aligned} (\dot{m}_{in})_x &= \rho \times A \times v = \rho \times \dot{m} \\ &= \rho \times (dz \times dy) \times u \end{aligned}$$

$$(\dot{m}_{out}) = \dot{m}_x in + \frac{\partial \dot{m}_x}{\partial x} x dx$$

$$\dot{m}_{stored} \text{ in } x\text{-direction} = (\dot{m}_{in})_x - (\dot{m}_{out})_x$$

$$= (\dot{m}_{in})_x - \left\{ (\dot{m}_{in})_x + \frac{\partial \dot{m}_x}{\partial x} x dx \right\}$$

$$(\dot{m}_{stored})_x = - \frac{\partial \dot{m}_x}{\partial x} dx$$

$$\dot{m}_x = \rho x (dy \times dz) \times u$$

$$(\dot{m}_{stored})_x = - \frac{\partial}{\partial x} (\rho (dy \times dz) u) dx$$

$$(\dot{m}_{stored})_x = - \frac{\partial}{\partial x} \rho (dx \cdot dy \cdot dz) \times u$$

Similarly $\dot{m}_{stored}$ along y & z co-ordinate axis

$$(\dot{m}_{stored})_y = - \frac{\partial}{\partial y} \rho (dx \cdot dy \cdot dz) \times v$$

$$(\dot{m}_{stored})_z = - \frac{\partial}{\partial z} \rho (dx \cdot dy \cdot dz) \times w$$

$$\text{Total mass stored } \dot{m} = \frac{d(m)}{dt}$$

$$\Rightarrow \frac{d}{dt} (\rho x dx dy dz) \quad (2)$$

$$\Sigma \text{ total mass stored in } (x, y, z) = \text{total mass stored.}$$

$$\Rightarrow - \frac{\partial}{\partial x} \rho (dx dy dz) u - \frac{\partial}{\partial y} \rho (dx dy dz) v - \frac{\partial}{\partial z} \rho (dx dy dz) w$$

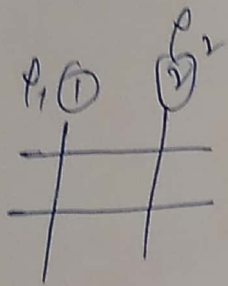
$$\Rightarrow -\frac{\partial}{\partial x}(\rho u) - \frac{\partial}{\partial y}(\rho v) - \frac{\partial}{\partial z}(\rho w) = \frac{d\rho}{dt}$$

Where ρ = mass density.

$$\therefore \Rightarrow \boxed{\frac{d\rho}{dt} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0}$$

General continuity equation

if flow field satisfy continuity equation then only flow is feasible else not.



$$\left(\frac{d\rho}{dt} \right)$$

$$d\rho = (\rho_2 - \rho_1) \neq 0$$

$\hookrightarrow \rho$ Not constant.
 $\Rightarrow$ changing.
 $\Rightarrow$ compressible.

* if $d\rho = 0$ ($\rho_1 = \rho_2$) = 0

$\hookrightarrow$ incompressible

$$\Rightarrow \frac{d\rho}{dt} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0$$

$$\Rightarrow \frac{d\rho}{dt} + \rho \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right) + u \frac{\partial \rho}{\partial x} + v \frac{\partial \rho}{\partial y} + w \frac{\partial \rho}{\partial z} = 0$$

* for steady flow

$$\left\{ \begin{array}{l} \frac{d\rho}{dt} = 0 \\ \left(\frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} \right) = 0 \end{array} \right.$$

at any broad section
 flow properties
 are constant.

* For incompressible flow

$\rho = \text{constant}$ i.e. it is not changing

$$\Rightarrow \rho \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right) = 0$$

$$\Rightarrow \rho \neq 0 \quad \checkmark \quad \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad \checkmark$$

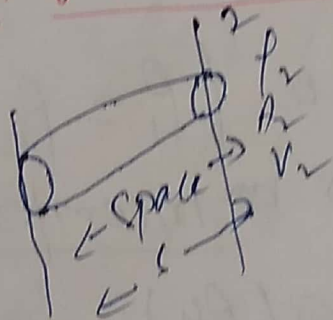
constant
not zero.

$\Rightarrow$ for steady & incompressible flow.

$$\boxed{\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0} \quad (3-D)$$

$$\Rightarrow (2-D) \quad \left(\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} \right) = 0$$

* Continuity equation for one dimensional flow



$$\Rightarrow \frac{dp}{dt} + \frac{\partial (\rho v)}{\partial s} = 0$$

$$\Rightarrow \frac{dp}{dt} + \frac{\partial (\dot{m})}{\partial s} = 0$$

$$\Rightarrow \frac{dp}{dt} + \frac{\partial (\rho A v)}{\partial s} = 0$$

$\rho A v = \dot{m}$
rate of
change of mass
(kg/sec)

$\hookrightarrow$ General equation for one dimensional flow.

Steady flow

$$\frac{dp}{dt} = 0$$

$$\frac{\partial(\rho v)}{\partial t} = 0$$

i.e

$$\rho v = \text{constant.}$$

$$\rho_1 A_1 v_1 = \rho_2 A_2 v_2$$

→ for steady flow only.

* For steady and incompressible flow.

$$\Rightarrow \rho = \text{constant} = \rho_1 = \rho_2 \quad \left| \quad \frac{d\rho}{dt} = 0. \right.$$

u.v.g

$$A_1 v_1 = A_2 v_2$$

↓ incompressible

→ at any particular section.

Q for steady and incompressible flow.

$$\vec{v} = (2xy^3 - x^2y)\hat{i} + (xy^2 - \frac{3}{4}y^4)\hat{j}$$

(value)

find λ .

soln

$$\vec{v} = u\hat{i} + v\hat{j} \quad \left\{ \begin{array}{l} u = 2xy^3 - x^2y \\ v = xy^2 - \frac{3}{4}y^4 \end{array} \right.$$

⇒ the given flow field must satisfy continuity equation.

for 2-D ⇒ $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$

$$\frac{\partial}{\partial x} (2xy^3 - x^2y) = (2y^3 - 2xy)$$

Similarly

$$\frac{\partial v}{\partial y} = \frac{\partial}{\partial y} (xy^2 - \frac{3}{4}y^4)$$

$$= (x \cdot 2y - \frac{3}{4} \cdot 4y^3)$$

$$\frac{\partial v}{\partial y} = (2xy - 3y^3)$$

$$\Rightarrow (2y^3 - 2xy) + (2xy - 3y^3) = 0$$

$$2y^3 = 3y^3$$

$$\boxed{1 = 3}$$