

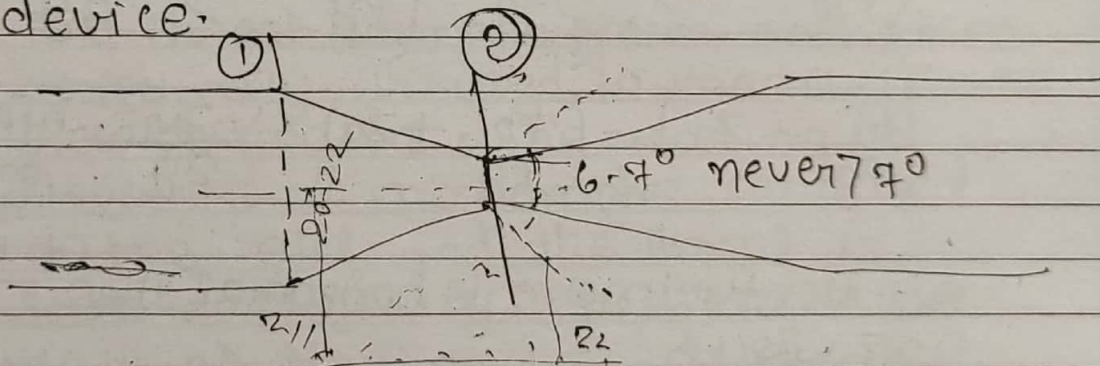
$$\frac{V_2}{V_1} = \sqrt{9} = 3$$

$$\left[\frac{V_2}{V_1} = \frac{3}{1} \right] \text{ Ans}$$

Application of Bernoulli's equation:

① Venturimeter →

venturimeter is a device which is used for finding out the discharge. It is a converging and diverging cross sectional device.



In venturimeter the length of diverging section is greater than that of converging section. Generally the diverging angle is kept less than 7° . In order to avoid flow separation because if we increase diverging angle, the diverging length will be decreased and hence flow separation will occur and hence direction of flow is ~~reverse~~ will be reversed. So the diverging angle should be less than converging angle.

It consists of three parts

(i) converging section

(ii) Throat.

(iii) diverging section

Applying Bernoulli's eqⁿ at the inlet venturimeter i.e. at section (1) and at the throat of venturimeter i.e. at section (2).

$$\frac{P_1}{\rho g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{v_2^2}{2g} + z_2$$

$$\left(\frac{P_1}{\rho g} + z_1 \right) + \frac{v_1^2}{2g} = \left(\frac{P_2}{\rho g} + z_2 \right) + \frac{v_2^2}{2g}$$

$$\left(\frac{P_1}{\rho g} + z_1 \right) - \left(\frac{P_2}{\rho g} + z_2 \right) = \frac{v_2^2 - v_1^2}{2g} = h \text{ [Piezo head diff]}$$

if venturimeter is horizontal then

$$z_1 = z_2$$

$$\frac{P_1}{\rho g} - \frac{P_2}{\rho g} = \frac{v_2^2 - v_1^2}{2g} = h \text{ (pressure head diff)}$$

$$\Rightarrow \frac{v_2^2 - v_1^2}{2g} = h$$

$$\Rightarrow v_2^2 - v_1^2 = 2gh$$

(1)

$$\text{Now } Q = a_1 v_1 = a_2 v_2$$

$$z_1 v_1 = \frac{Q_1}{a_1} \text{ \& } v_2 = \frac{Q}{a_2}$$

~~Substituting~~ Substituting v_1 & v_2 in eqn
① we have

$$\left(\frac{Q}{a_2}\right)^2 - \left(\frac{Q}{a_1}\right)^2 = 2gh$$

$$\Rightarrow \frac{Q^2}{a_2^2} - \frac{Q^2}{a_1^2} = 2gh$$

$$\Rightarrow Q^2 \left[\frac{1}{a_2^2} - \frac{1}{a_1^2} \right] = 2gh$$

$$\Rightarrow Q^2 \left[\frac{a_1^2 - a_2^2}{a_1^2 a_2^2} \right] = 2gh$$

$$\Rightarrow Q^2 = \frac{a_1^2 a_2^2 \cdot 2gh}{a_1^2 - a_2^2}$$

$$\Rightarrow Q = \sqrt{\frac{a_1^2 a_2^2 \cdot 2gh}{a_1^2 - a_2^2}}$$

$$\Rightarrow Q = \frac{a_1 a_2 \sqrt{2gh}}{\sqrt{a_1^2 - a_2^2}}$$

$$\Rightarrow Q = \frac{a_1 a_2 \sqrt{2gh}}{\sqrt{a_1^2 - a_2^2}}$$

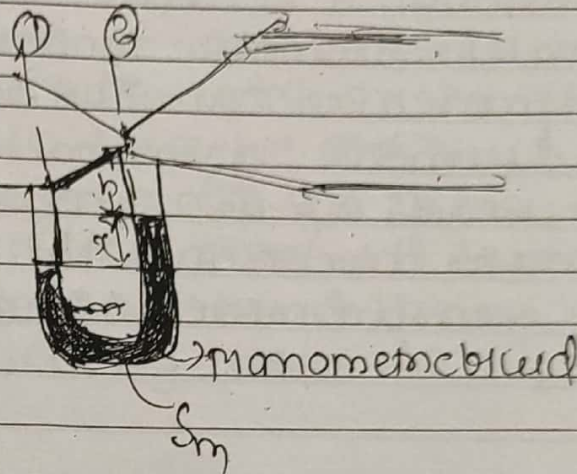
This is the required
expression for the discharge through
venturimeter.

Application

Discharge: Q
S.P. gravity: $S \rightarrow$

$$\frac{Q_1 > Q_2}{v_1 < v_2}$$

$$P_1 > P_2$$



$$P_1 + \rho g (H+x) - \rho_m g x - \rho g H = P_2$$

$$\Rightarrow \frac{P_1}{\rho g} + (H+x) - \frac{\rho_m g x}{\rho g} - \frac{\rho g H}{\rho g} = \frac{P_2}{\rho g}$$

$$\Rightarrow \frac{P_1}{\rho g} + (H+x) - \frac{\rho_m}{\rho} x - H = \frac{P_2}{\rho g}$$

$$\Rightarrow \frac{P_1}{\rho g} + \cancel{H} + x - \frac{\rho_m}{\rho} x - \cancel{H} = \frac{P_2}{\rho g}$$

$$\Rightarrow \frac{P_1}{\rho g} - \frac{P_2}{\rho g} = \frac{\rho_m}{\rho} x - x$$

$$\Rightarrow \frac{P_1}{\rho g} - \frac{P_2}{\rho g} = x \left(\frac{\rho_m}{\rho} - 1 \right)$$

$$h = x \left(\frac{\rho_m \cdot S}{S} - 1 \right)$$

coefficient of discharge (C_d):

It is defined as the ratio of actual discharge to the theoretical discharge.

$$C_d = \frac{Q_{act}}{Q_{th}}$$

$$\Rightarrow Q_{act} = C_d \cdot Q_{th}$$

$$Q_{act} = C_d \cdot a_1 a_2 \sqrt{2gh}$$

* C_d for venturimeter $\frac{\sqrt{a_1^2 - a_2^2}}{1} = 0.99$ to 0.99

Q. A horizontal venturimeter with an inlet and throat diameter 30cm and 15cm respectively is used to measure the flow of water. The reading of differential manometer connected to the inlet and the throat is 80cm of Mercury. Determine the rate of flow, i.e., discharge.
take $C_d = 0.98$

$$Q_{act} = C_d \cdot a_1 \cdot a_2 \cdot \sqrt{2gh}$$

Given, $D_1 = 30\text{cm}$

$D_2 = 15\text{cm}$

$$a_1 = \frac{\pi}{4} \times (30)^2 = 706.85 \text{ cm}^2$$

$$a_2 = \frac{\pi}{4} \times (15)^2 = 176.71 \text{ cm}^2$$

$$|12 = 10^{-3} \text{ m}^3|$$

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$$h = x \left[\frac{3m-1}{5} \right]$$

$$h = 20 [13.6 - 1]$$

$$252 \text{ cm}$$

Smc/3.6
er JS

$$Q_1 = \frac{C_d \cdot a_1 a_2 \sqrt{2gh}}{\sqrt{a_1^2 - a_2^2}}$$

$$= \frac{0.98 \times 706.85 \times 176.71 \times \sqrt{2 \times 9.8 \times 22}}{\sqrt{(706.85)^2 - (176.71)^2}}$$

$$\sqrt{(706.85)^2 - (176.71)^2}$$

$$= 12569.83 \text{ m}^3/\text{sec}$$

$$= 12.569 \text{ m}^3/\text{sec}$$

$$Cd = \frac{Q}{Q_2} \sqrt{\frac{2g h}{V_1^2 - V_2^2}}$$

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Q3.

A venturimeter of 20 millimetre throat diameter is installed in a horizontal pipe of 40 mill diameter. The fluid flowing is water. If the pressure difference between pipe and throat section is 30 kPa, find the velocity in pipe neglecting losses $P_1 - P_2 = 30000$
Pg

Q4

$$d_1 = 20 \text{ millimetre}$$

$$d_2 = 40 \text{ mill diameter}$$

$$Q_1 = Cd \cdot \frac{Q_2}{\sqrt{1 - \frac{d_1^4}{d_2^4}}} \sqrt{2gh}$$

$$Q_1 = \frac{Q_2}{\sqrt{1 - \left(\frac{d_1}{d_2}\right)^4}} \sqrt{2gh}$$

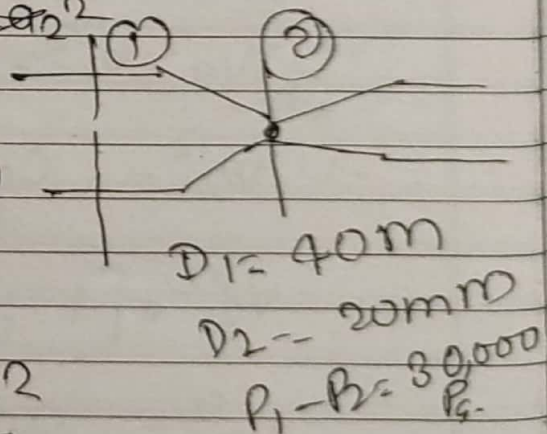
$$\frac{V_1^2 - V_2^2}{2} = \frac{P_1 - P_2}{\rho g}$$

$$\frac{P_1 - P_2}{\rho g} = \frac{V_2^2 - V_1^2}{2g}$$

$$\frac{30 \times 10^3}{1000} = \frac{V_2^2 - V_1^2}{2}$$

$$V_2^2 - V_1^2 = \frac{2 \times 30 \times 10^3}{1000}$$

$$V_2^2 - V_1^2 = 60$$



$$\left[\frac{0.9192 \times 10^{-11}}{\sqrt{0.9^2 - 0.2^2}} \right] \times \left[\frac{300 \times 10^3}{1} \right]$$

$$q_1 v_1 = q_2 v_2$$

$$\frac{q_1}{q_2} = \frac{v_2}{v_1}$$

$$\frac{\frac{\pi}{4} \times D_1^2}{\frac{\pi}{4} \times D_2^2} = \frac{v_2}{v_1}$$

$$= \frac{(40)^2}{(20)^2} = \frac{v_2}{v_1}$$

$$= \frac{1600}{400} = \frac{v_2}{v_1}$$

$$v_2 = 4v_1 \quad \text{--- (1)}$$

$$(4v_1)^2 - v_1^2 = 60$$

$$3v_1^2 = 60$$

$$v_1 = 2 \text{ m/s}$$

$$v_2 = 8 \text{ m/s}$$

$$16v_1^2 - v_1^2 = 60$$

$$15v_1^2 = 60$$

$$v_1^2 = \frac{60}{15}$$

$$v_1 = 2 \text{ m/s}$$

$$v_2 = 4v_1$$

$$v_2 = 4 \times 2$$

$$v_2 = 8 \text{ m/s}$$

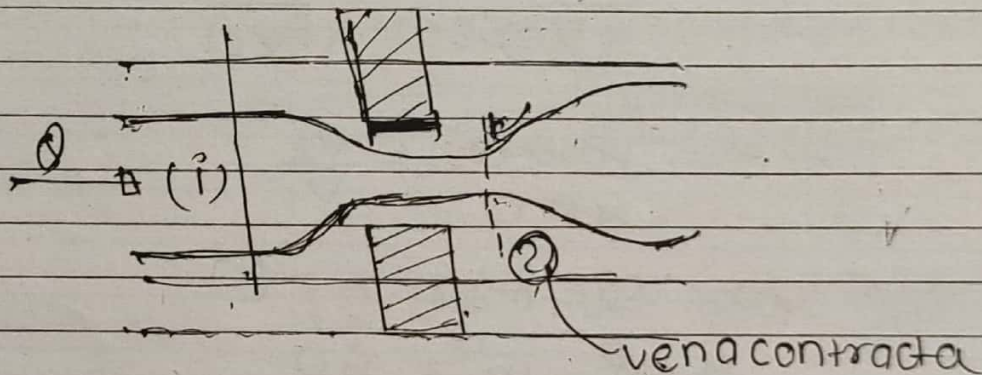
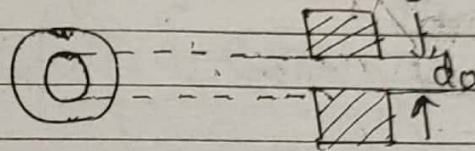
$$v_1 = 2 \text{ m/s}$$

$$v_2 = 8 \text{ m/s}$$

B

Orifice meter: →

It is used for finding out discharge and is based on the same principle as that of venturimeter and is the cheapest instrument for finding the discharge.



* Coefficient of contraction (C_c)

$$C_c = \frac{a_2}{a_0}$$

$$\therefore a_2 = C_c \cdot a_0$$

$$a_1 v_1 = a_2 v_2$$

$$a_1 v_1 = C_c \cdot a_0 \cdot v_2$$

$$v_1 = \frac{C_c \cdot a_0 \cdot v_2}{a_1}$$

Applying Bernoulli's eqⁿ between
① and ②.

$$\frac{P_1}{\rho g} + \frac{v_1^2}{2g} + z_1 = \frac{P_2}{\rho g} + \frac{v_2^2}{2g} + z_2$$

for horizontal pipe, $z_1 = z_2$

$$\frac{P_1}{\rho g} + \frac{v_1^2}{2g} = \frac{P_2}{\rho g} + \frac{v_2^2}{2g}$$

$$\therefore \frac{P_1}{\rho g} - \frac{P_2}{\rho g} = \frac{v_2^2}{2g} - \frac{v_1^2}{2g} = h \text{ (pressure head difference)}$$

$$\Rightarrow \frac{v_2^2}{2g} - \frac{v_1^2}{2g} = h$$

$$\therefore v_2^2 - v_1^2 = 2gh$$

$$\therefore v_2^2 - (C_c \frac{a_0}{a_1} v_2)^2 = 2gh$$

$$= v_2^2 \left[1 - C_c^2 \frac{a_0^2}{a_1^2} \right] = 2gh$$

$$\Rightarrow v_2^2 = \frac{2gh}{1 - C_c^2 \frac{a_0^2}{a_1^2}}$$

$$\Rightarrow v_2 = \frac{\sqrt{2gh}}{\sqrt{1 - \frac{C_c^2 a_0^2}{a_1^2}}}$$

Now,

discharge $Q = a_2 v_2$

$$Q = \frac{C_c \cdot a_0 \sqrt{2gh}}{\sqrt{1 - \frac{C_c^2 a_0^2}{a_1^2}}}$$

$$Q = \frac{C_c a_0 \sqrt{2gh} \times \sqrt{1 - \frac{a_0^2}{a_1^2}}}{\sqrt{1 - \frac{C_c^2 a_0^2}{a_1^2}} \times \sqrt{1 - \frac{a_0^2}{a_1^2}}}$$

$$\text{Eq 9b } C_d = \frac{C_c \sqrt{1 - \frac{a_0^2}{a_1^2}}}{\sqrt{1 - \frac{C_c^2 a_0^2}{a_1^2}}}$$

then

$$Q = \frac{C_d \cdot a_0 \sqrt{2gh}}{\sqrt{1 - \frac{a_0^2}{a_1^2}}}$$

$$Q = \frac{C_d \cdot a_0 \sqrt{2gh}}{\sqrt{a_1^2 - a_0^2}}$$

$$Q = \frac{C_d a_0 a_1 \sqrt{2gh}}{\sqrt{a_1^2 - a_0^2}}$$

(Eq 9c)

for orifice meter, the value of C_d is $\boxed{0.68 \text{ to } 0.76}$

$$C_d = C_c \cdot \frac{\sqrt{1 - \frac{a_0^2}{a_1^2}}}{\sqrt{1 - C_c^2 \frac{a_0^2}{a_1^2}}}$$

in some books

the term

$$\frac{\sqrt{1 - \frac{a_0^2}{a_1^2}}}{\sqrt{1 - C_c^2 \frac{a_0^2}{a_1^2}}}$$

is termed

$$\frac{\sqrt{1 - \frac{a_0^2}{a_1^2}}}{\sqrt{1 - C_c^2 \frac{a_0^2}{a_1^2}}}$$

as coefficient of velocity

so $\boxed{C_d = C_c \cdot C_v}$

Q1. An orifice metre is being used for measuring flow rate of liquid in a pipeline source a pressure diff of 2 metre of water column when the flow is 1. If the flow rate is double, the pressure head difference in m is

(a) 2 (b) 8 (c) 4 (d) 16

Sol.

$$\frac{P_1}{\rho g} - \frac{P_2}{\rho g} = \frac{V_2^2}{2g} - \frac{V_1^2}{2g} = h \text{ (head)}$$

$$Q = \frac{C_d a_0 a_1 \sqrt{2gh}}{\sqrt{a_1^2 - a_0^2}}$$

$$Q \propto \sqrt{h}$$

$$Q_1 = K \sqrt{h_1}$$

$$\frac{Q_1}{Q_2} = \sqrt{\frac{h_1}{h_2}}$$

$$Q = K \sqrt{h}$$

$$Q_1 = K \sqrt{h_1} \quad (I)$$

$$Q_2 = K \sqrt{h_2} \quad (II)$$

$$\frac{Q_1}{Q_2} = \sqrt{\frac{h_1}{h_2}}$$

$$\frac{1}{2} = \sqrt{\frac{h_1}{h_2}}$$

Squaring

$$\frac{1}{4} = \frac{h_1}{h_2}$$

$$h_2 = 4h_1$$

Q2.

An orifice metre with $C_d = 0.61$ is substituted by venturimeter with $C_d = 0.98$ in a pipe line carrying oil having same throat diameter as that of orifice metre. for the same flow rate. What will be ratio of pressure drops for venturimeter to that orifice metre.

Sol

$$Q = \frac{C_d \cdot a_1 a_2 \sqrt{2gh}}{\sqrt{a_1^2 - a_2^2}}$$

$$(C_d)_v = 0.98 \quad (C_d)_o = 0.61$$

$$D_t = D_o$$

$$a_t = a_o$$

$$a_2 = a_o$$

$$Q_v = Q_o$$

$$\frac{(C_d)_v a_1 a_2 \sqrt{2gh_v}}{\sqrt{a_1^2 - a_2^2}} = \frac{(C_d)_o a_1 a_o \sqrt{2gh_o}}{\sqrt{a_1^2 - a_o^2}}$$

$$\frac{0.98}{0.61} = \frac{\sqrt{2gh_o}}{\sqrt{2gh_v}}$$

$$\frac{(C_d)_v}{(C_d)_o} = \frac{\sqrt{2gh_o}}{\sqrt{2gh_v}}$$

$$\left(\frac{0.98}{0.61} \right)^2 = \frac{h_o}{h_v}$$

$$\frac{h_o (0.98^2)}{h_v (0.61^2)}$$

$$\frac{h_o}{h_v} =$$

$$\frac{h_v}{h_u} = \frac{0.61^2}{0.98^2}$$

$$\frac{(P_1 - P_2) V}{\rho \theta} = \frac{0.61^2}{0.98^2}$$

$$\frac{(P_1 - P_2) \theta}{\rho \theta}$$

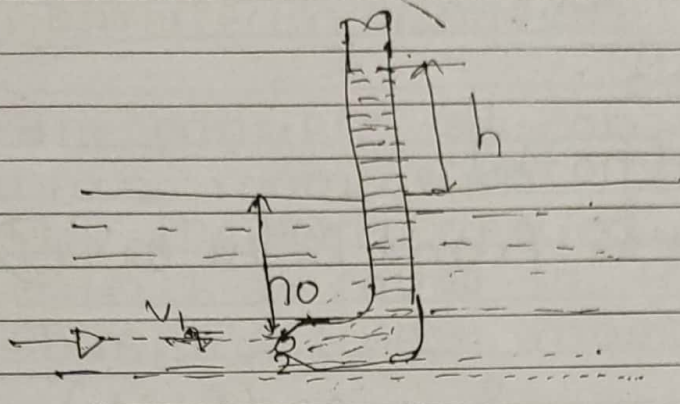
$$\frac{(P_1 - P_2) V}{(P_1 - P_2) \theta} = \frac{0.61^2}{0.98^2} \quad (P_2)$$

~~P + P_0~~

*

Pitot tube: → It is based on the principle that if the velocity of flow at any point becomes zero the pressure is increased due to change of K.E into pressure energy.

Pitot tube is used for finding out velocity of flow at any point in a pipe or channel.



consider two points 1 and 2 at the same level in such a way that point 2 is just the inlet of the pitot tube and point 1 is far away from the tube. Since at 2 velocity becomes zero so P_2 is increased and the liquid rises in the pitot tube as shown in the figure.

Applying Bernoulli's equation b/w pt ① and ② for horizontal pipe, we have

$$\frac{P_1}{\omega} + \frac{v_1^2}{2g} = \frac{P_2}{\omega} + \frac{v_2^2}{2g}$$

since at 2, velocity: 0

so, $v_2 = 0$ hence the above eqⁿ becomes

$$\frac{P_1}{\omega} + \frac{v_1^2}{2g} = \frac{P_2}{\omega} \quad \text{--- (1)}$$

↓
↓
↓

Static head
Kinetic head
Stagnation head.

Here,

$$P_1 = \rho g h_0$$

$$P_2 = \rho g (h_0 + h)$$

substituting P_1 and P_2 in eqn (1)
we get,

Eqn.

$$\frac{\rho g h_0}{\omega} + \frac{v_1^2}{2g} = \frac{\rho g (h_0 + h)}{\omega}$$

Putting $\omega = \rho g = \rho \cdot \omega \cdot t$

$$\frac{\cancel{\rho} g h_0}{\cancel{\rho} g} + \frac{v_1^2}{2g} = \frac{\cancel{\rho} g (h_0 + h)}{\cancel{\rho} g}$$

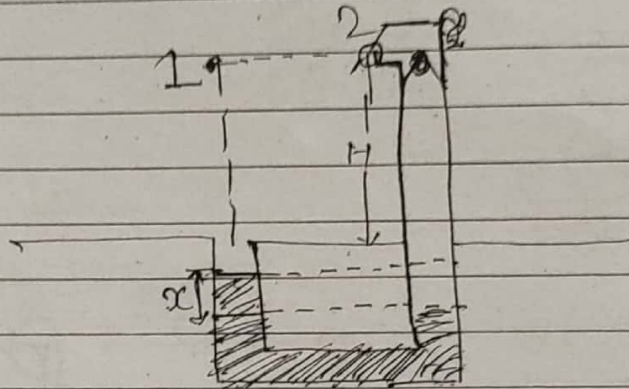
$$\Rightarrow h_0 + \frac{v_1^2}{2g} = h_0 + h$$

$$\Rightarrow \frac{v_1^2}{2g} = h$$

$$\Rightarrow v_1^2 = 2gh$$

$$v_1 = \sqrt{2gh}$$

velocity in pipes:



② Applying Bernoulli's equation at 1 and 2

$$\frac{P_1}{\rho} + \frac{v_1^2}{2g} = \frac{P_2}{\rho} + \frac{v_2^2}{2g}$$

g.b. $v_1 = v_2 = 0$ then

$$\frac{P_1}{\rho} + \frac{v_1^2}{2g} = \frac{P_2}{\rho} \quad \text{--- (ii)}$$

from balancing of fluid column technique

$$P_1 + \rho g H + \rho_m g x - \rho g (H+x) = P_2$$

dividing by ρg

$$\frac{P_1}{\rho g} + \frac{\cancel{\rho g H}}{\cancel{\rho g}} + \frac{\rho_m g x}{\rho g} - \frac{\rho g (H+x)}{\cancel{\rho g}} = \frac{P_2}{\rho g}$$

$$\frac{P_1}{\rho g} + \cancel{H} + \frac{\rho_m x}{\rho} - \cancel{H} - \cancel{x} = \frac{P_2}{\rho g}$$

$$\Rightarrow \frac{P_1}{\omega} + \frac{\rho_m x}{s} - x = \frac{P_2}{\omega}$$

$$\Rightarrow \frac{P_1}{\omega} = \frac{P_2}{\omega} + x \left(1 - \frac{\rho_m}{s} \right)$$

Substituting the ~~putting the~~
 $\frac{P_2}{\omega}$ in eqn (1)

$$\cancel{\frac{P_2}{\omega}} + x \left(1 - \frac{\rho_m}{s} \right) + \frac{v_1^2}{2g} = \cancel{\frac{P_2}{\omega}}$$

$$\frac{v_1^2}{2g} = x \left(\frac{\rho_m}{s} - 1 \right)$$

$$\Rightarrow v_1 = \sqrt{2gx \left(\frac{\rho_m}{s} - 1 \right)}$$

9. A Pitot tube is used to measure velocity of water using differential gauge which contains manometric fluid of specific gravity 1.4. ~~find~~ .9b the velocity of water is 1.2 m/sec find manometric fluid deflection.

Soln

$$v_1 = \sqrt{2gx \left(\frac{\rho_m}{s} - 1 \right)}$$

$$(1.2)^2 = \sqrt{2gx \left(\frac{1.4}{1} - 1 \right)}$$

$$2gx (0.4) = (1.2)^2$$

$$x = \frac{(1.2)^2}{2g \times 0.4} = 0.183 \text{ m}$$